

Distributed MPC for tracking.

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March 6, 2013

Outline

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- Problem statement

Cooperative MPC for tracking

- Cooperative MPC for tracking

- Warm start algorithm

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- The 4 tanks plant

- The distributed model

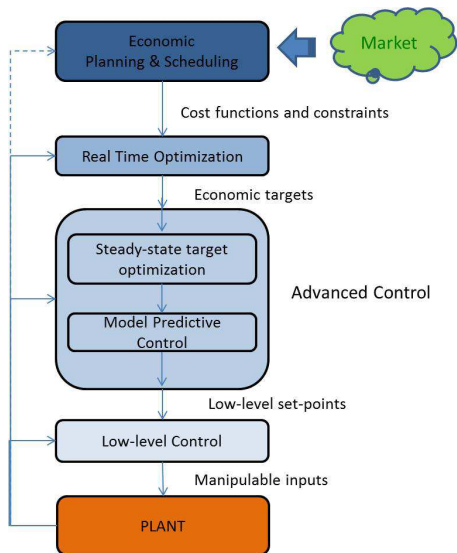
- Experiment

Concluding remarks

- Summary

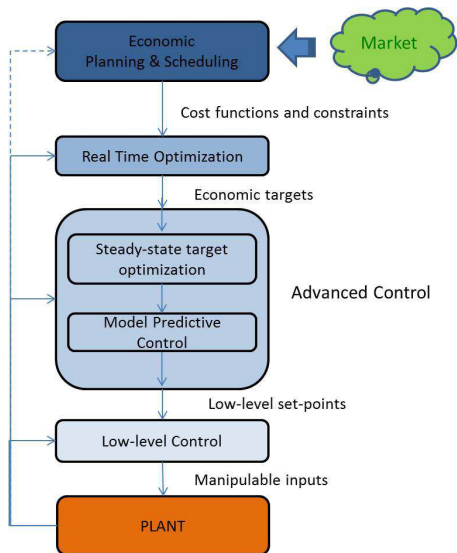
- References

Large scale systems control structure



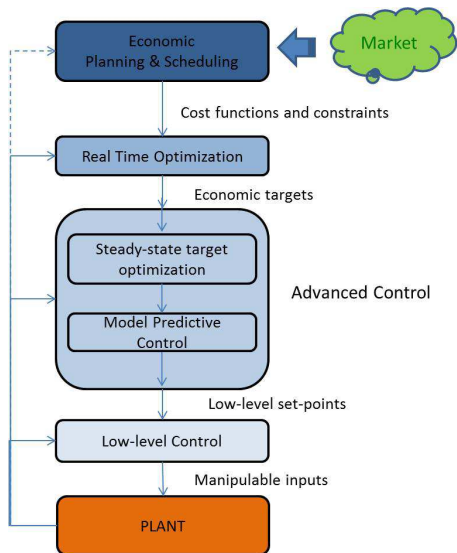
1. Market-oriented decision making.
2. RTO for the economic optimization.
3. Advanced control: MPC.
4. SSTO: extra optimization level. It reduces the gap between RTO and MPC.
5. Low level control and feedback from the plant.

Large scale systems control structure



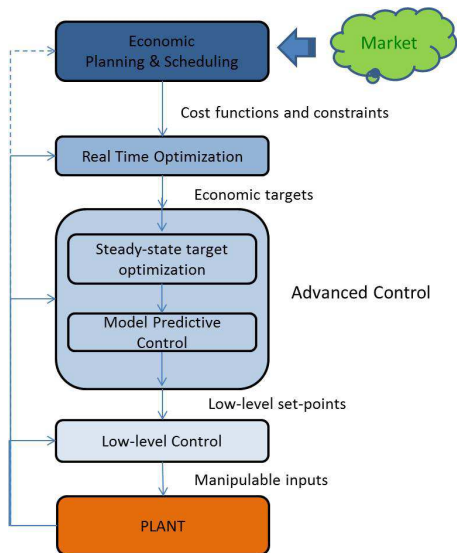
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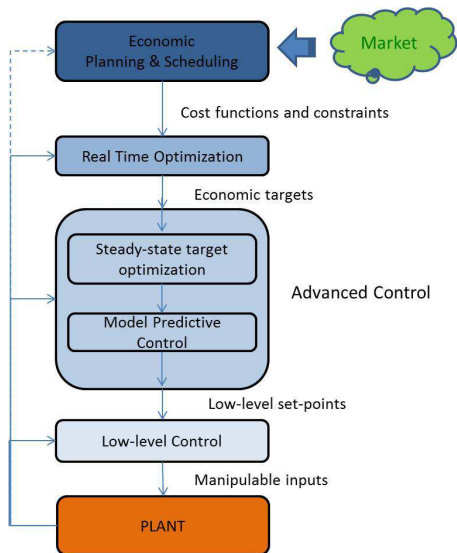
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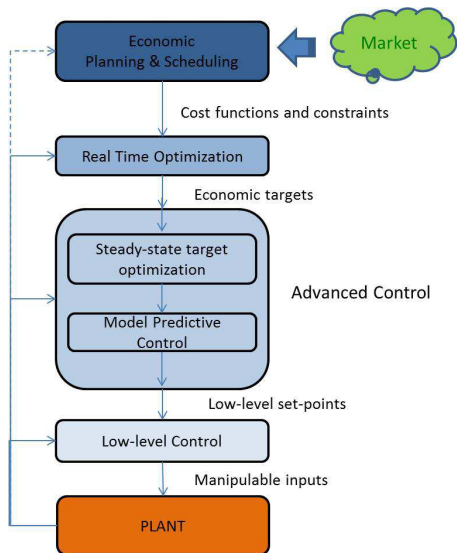
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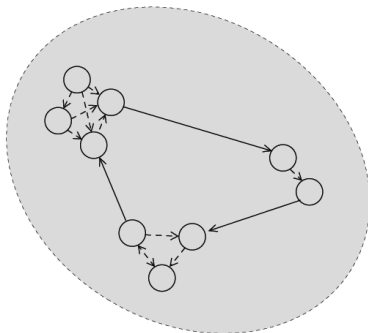
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Different interconnected units

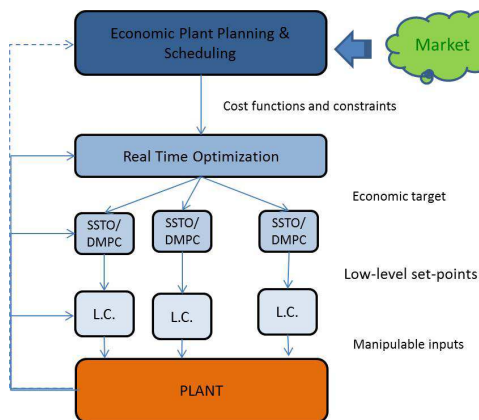


1. Centralized control: high computational burden.
2. Decentralize control: interactions between the different subsystems not considered.
3. Distributed control: "*agents share open-loop information in order to improve closed-loop performance*". (Rawlings & Mayne, 2009).

Different distributed control strategies

1. **Noncooperative control**: agents' objectives compete (Camponogara et al., 2002; Dunbar, 2007).
 - ▶ **Nash equilibrium**: neither player can improve his position given the other players' decision.
2. **Dual decomposition**: Lagrange multipliers as prices in a market mechanism, to achieve an agreement (Rantzer, 2009; Negenborn et al., 2009).
3. **Cooperative control**: agents share a common objective, which can be considered as the overall plant objective (Rawlings & Mayne, 2009; Stewart et al., 2010).
 - ▶ **Negotiation**: agents make different proposals, one of them is chosen based on some criterion (Maestre et al., 2011).

Cooperative MPC para tracking (Ferramosca et al., 2013)



1. SSSO + MPC in one optimization loop.
2. Distributed dynamic optimization.
3. Centralized target problem.
4. Convergence to centralized optimum.

Problem statement

- ▶ Consider a system described by a discrete time invariant linear system:

$$\begin{aligned}x^+ &= Ax + Bu \\ y &= Cx + Du\end{aligned}\tag{1}$$

- ▶ $x \in \mathbb{R}^n$, $u \in \mathbb{R}^m$, $y \in \mathbb{R}^p$, x^+ is the successor state.
- ▶ Hard constraints on state and control input:

$$(x(k), u(k)) \in \mathcal{Z} = \mathcal{X} \times \mathcal{U}$$

- ▶ $\mathcal{X} \subset \mathbb{R}^n$ and $\mathcal{U} \subset \mathbb{R}^m$ compact convex polyhedra containing the origin in their interior.

Assumption

The pair (A,B) is stabilizable and the state is measured at each sampling time.

Problem statement (2)

- ▶ Steady state: (x_s, u_s, y_s) such that $x_s = Ax_s + Bu_s$, and $y_s = Cx_s + Du_s$ and

$$\begin{bmatrix} A - I_n & B & \mathbf{0}_{p,1} \\ C & D & -I_p \end{bmatrix} \begin{bmatrix} x_s \\ u_s \\ y_s \end{bmatrix} = \begin{bmatrix} \mathbf{0}_{n,1} \\ \mathbf{0}_{p,1} \end{bmatrix} \quad (2)$$

- ▶ This parametrization is possible if and only if $\text{rank} = n + p$. Otherwise, use a linear combination of a vector $\theta \in \mathbb{R}^m$ (Limon et al., 2008).
- ▶ Sets of admissible equilibrium states, inputs and outputs:

$$\mathcal{Z}_s = \{(x, u) \in \mathcal{X} \times \mathcal{U} \mid x = Ax + Bu\} \quad (3)$$

$$\mathcal{X}_s = \{x \in \mathcal{X} \mid \exists u \in \mathcal{U} \text{ such that } (x, u) \in \mathcal{Z}_s\} \quad (4)$$

$$\mathcal{Y}_s = \{y = Cx + Du \mid (x, u) \in \mathcal{Z}_s\} \quad (5)$$

Distributed partition of the plant

- ▶ System (1) can be partitioned in M subsystems of the form:

$$\begin{aligned}x_i^+ &= A_i x_i + \sum_{j=1}^M \bar{B}_{ij} u_j \\ y_i &= C_i x_i + \sum_{j=1}^M \bar{D}_{ij} u_j\end{aligned}\quad (6)$$

where $x_i \in \mathbb{R}^{n_i}$, $u_j \in \mathbb{R}^{m_j}$, $y_i \in \mathbb{R}^{p_i}$, $A_i \in \mathbb{R}^{n_i \times n_i}$, $\bar{B}_{ij} \in \mathbb{R}^{n_i \times m_j}$, $C_i \in \mathbb{R}^{p_i \times n_i}$ and $\bar{D}_{ij} \in \mathbb{R}^{p_i \times m_j}$.

- ▶ Without loss of generality, it is considered that

$$u = (u_1, \dots, u_M)$$

- ▶ For the two players game:

$$\begin{bmatrix} x_1 \\ x_2 \end{bmatrix}^+ = \begin{bmatrix} A_1 & \\ & A_2 \end{bmatrix} \begin{bmatrix} x_1 \\ x_2 \end{bmatrix} + \begin{bmatrix} \bar{B}_{11} \\ \bar{B}_{21} \end{bmatrix} u_1 + \begin{bmatrix} \bar{B}_{12} \\ \bar{B}_{22} \end{bmatrix} u_2$$

Cooperative MPC for tracking

Players share a common objective: overall plant cost function.

- ▶ Cooperative MPC (Stewart et al., 2010):

$$V_N^c(\mathbf{x}, \mathbf{y}_t; \mathbf{u}) = \sum_{j=0}^{N-1} \|\mathbf{x}(j) - \mathbf{x}_t\|_Q^2 + \|\mathbf{u}(j) - \mathbf{u}_t\|_R^2 + \|\mathbf{x}(N) - \mathbf{x}_t\|_P^2$$

- ▶ Cooperative MPC for tracking (Ferramosca et al., 2013):

$$V_t(\mathbf{x}, \mathbf{y}_t; \mathbf{u}, \hat{\mathbf{y}}_s) = \sum_{j=0}^{N-1} \|\mathbf{x}(j) - \hat{\mathbf{x}}_s\|_Q^2 + \|\mathbf{u}(j) - \hat{\mathbf{u}}_s\|_R^2 + \|\mathbf{x}(N) - \hat{\mathbf{x}}_s\|_P^2 + V_O(\hat{\mathbf{y}}_s, \mathbf{y}_t)$$

Features:

- ▶ Artificial steady state and input as decision variables.
- ▶ Penalizing the deviation of the predicted trajectory with the artificial steady conditions.
- ▶ Centralized offset-cost function.
- ▶ The system is stirred to *any* equilibrium point in N steps.

Optimization problem (2 players game)

Each i -th agent solves an iterative decentralized optimization problem

$$\begin{aligned}(\mathbf{u}_i^*, \hat{\mathbf{y}}_{s,i}^*) &= \arg \min_{\mathbf{u}_i, \hat{\mathbf{y}}_{s,i}} V_i(x, y_i; \mathbf{u}, \hat{\mathbf{y}}_s) \\ \text{s.t. } x_q(j+1) &= A_q x_q(j) + \sum_{\ell=1}^2 B_{q\ell} u_\ell(j), \quad q \in \mathbb{I}_{1,2} \\ x(0) &= (x_1, x_2), \\ \mathbf{u}_\ell &= \mathbf{u}_\ell^{[\rho]}, \quad \ell \in \mathbb{I}_{1,2} \setminus i, \\ x(j) &\in \mathcal{X}, \\ (u_1(j), u_2(j)) &\in \mathcal{U}, \quad j = 0, \dots, N-1 \\ (x(N), \hat{\mathbf{y}}_s) &\in \Omega_{t,K}\end{aligned}$$

$$\begin{aligned}\mathbf{u}_1^{[\rho+1]} &= w_1 \mathbf{u}_1^* + w_2 \mathbf{u}_1^{[\rho]} \\ \mathbf{u}_2^{[\rho+1]} &= w_1 \mathbf{u}_2^{[\rho]} + w_2 \mathbf{u}_2^* \\ \hat{\mathbf{y}}_s^{[\rho+1]} &= w_1 \hat{\mathbf{y}}_{s,1}^*(x, \mathbf{u}_2^{[\rho]}) \\ &\quad + w_2 \hat{\mathbf{y}}_{s,2}^*(x, \mathbf{u}_1^{[\rho]}) \\ w_1 + w_2 &= 1 \quad w_1, w_2 > 0\end{aligned}$$

Stop:

- ▶ $\mathbf{u}_1^{[\rho+1]} = \mathbf{u}_1^{[\rho]}$
- ▶ $\rho = \bar{\rho}$

- ▶ Centralized invariant set for tracking (Limon et al., 2008; Ferramosca et al., 2009).
- ▶ Jacobi (simultaneous) solution (Bertsekas & Tsitsiklis, 1997, pp. 219-223) and convex update.
- ▶ Iterate $(\mathbf{u}_1^{[0]}, \mathbf{u}_2^{[0]})$: *warm-start* algorithm.

The *warm start* algorithm (Ferramosca et al., 2013)

1. First candidate:

$$\tilde{\mathbf{u}}(k+1) = \{u(1; k), \dots, u(N-1; k), u_c(N)\}$$

where

$$u_c(N) = Kx(N) + L\hat{y}_s^*(k)$$

centr. terminal control law.

2. Second candidate:

$$\hat{\mathbf{u}}(k+1) = \{\hat{u}_c(0), \dots, \hat{u}_c(N-1)\}$$

where

$$\hat{x}(0) = x(k+1)$$

$$\hat{x}(j+1) = (A+BK)\hat{x}(j) + BL\hat{y}_s^*(k), \quad j \in \mathbb{I}_{1:N-2}$$

$$\hat{u}_c(j) = K\hat{x}(j) + L\hat{y}_s^*(k)$$

3. **IF** $(x(k+1), \hat{y}_s^*(k)) \in \Omega_{t,K}$ **AND** $V_N(x(k+1), y_t, \hat{\mathbf{u}}) \leq V_N(x(k+1), y_t, \tilde{\mathbf{u}})$
SET

$$\mathbf{u}(k+1)^{[0]} = (\hat{\mathbf{u}}(k+1), \hat{y}_s^*(k))$$

ELSE

$$\mathbf{u}(k+1)^{[0]} = (\tilde{\mathbf{u}}(k+1), \hat{y}_s^*(k))$$

Remark

- ▶ When $(x(k+1), \hat{y}_s^*(k)) \in \Omega_{t,K}$, the *distr. MPC* should work better than the *centralized terminal controller*.
- ▶ If not, i.e. $V_N(x(k+1), \hat{\mathbf{u}}) \leq V_N(x(k+1), \tilde{\mathbf{u}})$, choose the *centralized terminal control law as warm start*.

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Properties

Stability: for any y_t , closed-loop A-stable and converges to

$$y_s = \arg \min_{\hat{y}_s \in \lambda \mathcal{Y}_s} V_O(\hat{y}_s, y_t)$$

- ▶ Convexity.
- ▶ Recursive feasibility: warm start and centralized terminal constraint.
- ▶ Sub-optimal MPC (Scokaert et al., 1999).

Optimality: for any y_t , centralized optimum.

- ▶ For coupled and uncoupled constraints. For any $\bar{\rho} \geq 1$.
- ▶ Centralized offset cost function (SSTO).
- ▶ Warm start.

Larger domain of attraction: set of initial conditions admissibly steerable to *any* steady state.

- ▶ Constraints do not depend on y_t .

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The 4 tanks plant¹

Interesting features:

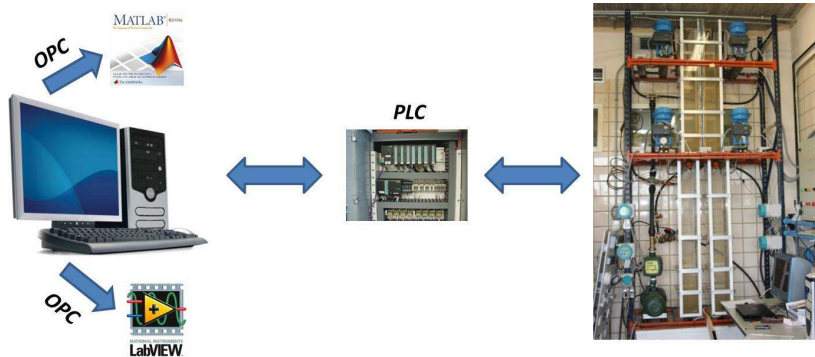
1. All the states are measurable.
2. The outputs are strongly coupled.
3. The system is nonlinear.
4. The states and inputs are constrained.

$$\begin{aligned}\frac{dh_1}{dt} &= -\frac{a_1}{A_1} \sqrt{2gh_1} + \frac{a_3}{A_1} \sqrt{2gh_3} + \frac{\gamma_a}{A_1} q_a \\ \frac{dh_2}{dt} &= -\frac{a_2}{A_2} \sqrt{2gh_2} + \frac{a_4}{A_2} \sqrt{2gh_4} + \frac{\gamma_b}{A_2} q_b \\ \frac{dh_3}{dt} &= -\frac{a_3}{A_3} \sqrt{2gh_3} + \frac{(1-\gamma_b)}{A_3} q_b \\ \frac{dh_4}{dt} &= -\frac{a_4}{A_4} \sqrt{2gh_4} + \frac{(1-\gamma_a)}{A_4} q_a\end{aligned}$$



¹Detailed description of the plant and simulation model at

The 4 tanks plant: setup at Univ. de Sevilla



- ▶ 4 pressure sensors: Siemens Sitrans P 7MF4020.
- ▶ 4 electromagnetic flowmeters Siemens.
- ▶ 4 pneumatic control valves: Siemens VC 101.
- ▶ Pumping system: Pump SACI K41T 4HP.
- ▶ Maximum Levels detected by floats switches.
- ▶ PLC: Siemens S7-200.

The 4 tanks plant: LabVIEW[®]

Labview OPC client todo.vi

File Edit Operate Tools Browse Window Help

Todo Sinoptico Caudal12 Caudal34 Alturas

Visualización del proceso

Tiempo de muestreo: 500

a1pu	a2pu	a3pu	a4pu	Volumen Máximo
0,171	0,149	0,219	0,077	
hsf1	hsf2	hsf3	hsf4	Suma
0,172	0,134	0,051	0,004	0,488
hf1	hf2	hf3	hf4	
0,141	0,102	0,049	0,004	
qsf1	qsf2	qsf3	qsf4	Suma Q
0,552	0,550	0,488	0,396	1,99
qf1	qf2	qf3	qf4	
0,536	0,538	0,494	0,387	
ref1	ref2	ref3	ref4	
0,56	0,58	0,49	0,40	
K1	K2	K3	K4	
1,00	1,00	1,00	1,00	
Ti1	Ti2	Ti3	Ti4	
0,08	0,08	0,08	0,08	
Td1	Td2	Td3	Td4	
0,00	0,00	0,00	0,00	

Bomba Activada Recirculación cerrada Protección activada
 PIDs Activados Rectas Activadas

Valor de las constantes de los filtros: bh: 0,75 bq: 0,75
 Valor del caudal máximo y mínimo de la protección de la bomba: Qmax: 1,00 Qmin: 0,75

Control de proceso

Bomba en marcha
 Válvula cerrada
 Montornización del byte de estado: Bomba on, Centrar válvula, Activar PIDs, Activar Rectas, Activar Protección, Filtro PID

Ref 4: 0,40
 Ref 3: 0,49
 Ref 2: 0,58
 Ref 1: 0,56

Escribir byte de estado Escribir referencias

Configuración PIDs

K1: 1,00 K2: 1,00 K3: 1,00 K4: 1,00
 Ti1: 0,08 Ti2: 0,08 Ti3: 0,08 Ti4: 0,08
 Td1: 0,00 Td2: 0,00 Td3: 0,00 Td4: 0,00

Escribir variables PIDs y los filtros

Filtros e histeresis

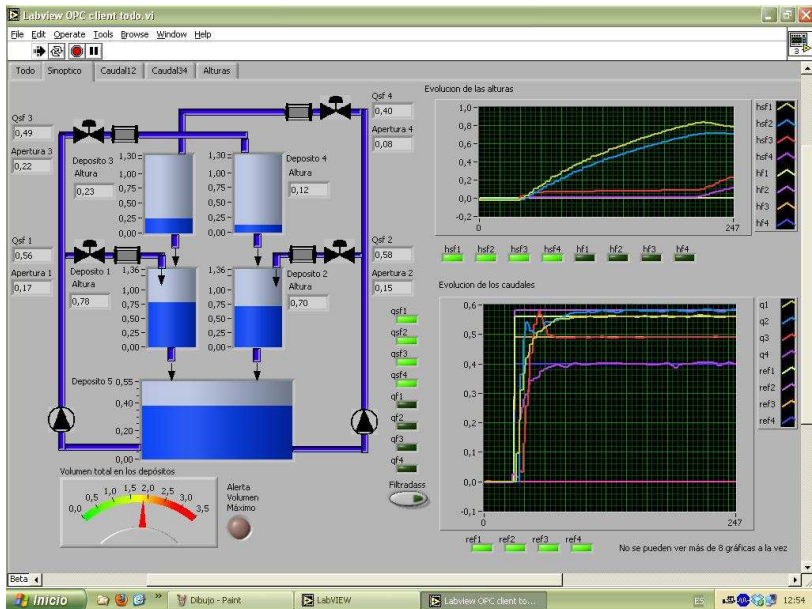
Escribir constantes filtro y caudales histeresis

bq: 0,75 bh: 0,75 Qmax: 1,00 Qmin: 0,75

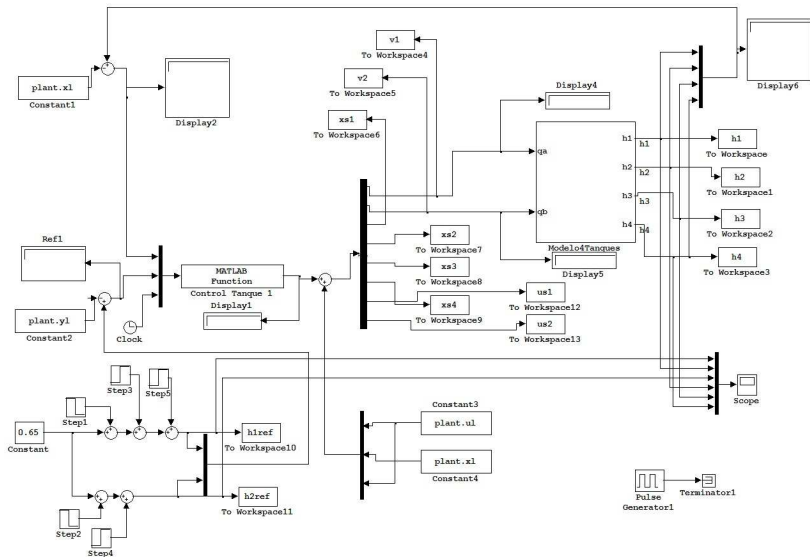
Beta

Inicio | Dibujo - Paint | LabVIEW | Labview OPC client to... | ES | 12:52

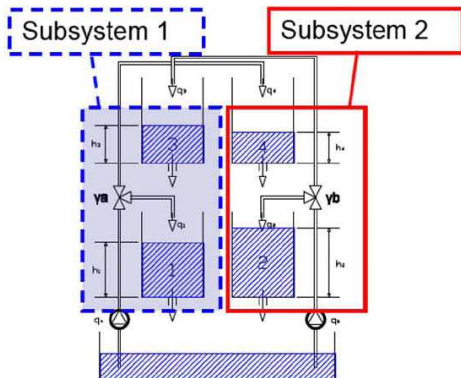
The 4 tanks plant: LabVIEW[®]



The 4 tanks plant: Simulink[®]



The distributed model



Linearization:

- ▶ $\bar{u}_0 = (1.63, 2)$.
- ▶ \bar{x}_0 as the levels s. t.
 $(x - \bar{x}_0) = A(x - \bar{x}_0) + B(u - \bar{u}_0)$.

Distributed model:

$$\frac{dx_1}{dt} = \begin{bmatrix} \frac{-1}{\tau_1} & \frac{A_3}{A_1 \tau_3} \\ 0 & \frac{-1}{\tau_3} \end{bmatrix} x_1 + \begin{bmatrix} \frac{\gamma_a}{A_1} \\ 0 \end{bmatrix} u_1 + \begin{bmatrix} 0 \\ \frac{(1-\gamma_b)}{A_3} \end{bmatrix} u_2$$

$$\frac{dx_2}{dt} = \begin{bmatrix} \frac{-1}{\tau_2} & \frac{A_4}{A_2 \tau_4} \\ 0 & \frac{-1}{\tau_4} \end{bmatrix} x_2 + \begin{bmatrix} 0 \\ \frac{(1-\gamma_a)}{A_4} \end{bmatrix} u_1 + \begin{bmatrix} \frac{\gamma_b}{A_2} \\ 0 \end{bmatrix} u_2$$

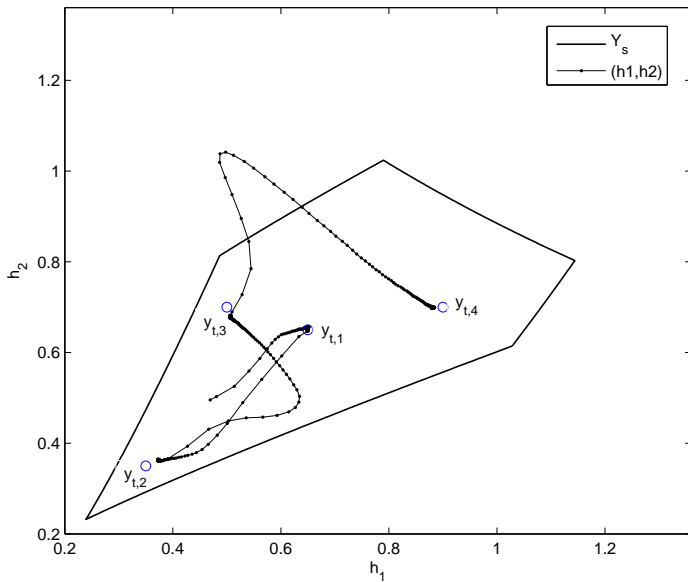
where $x_1 = (h_1, h_3)$, $x_2 = (h_2, h_4)$, $u_1 = q_a$ and $u_2 = q_b$.

Experiment

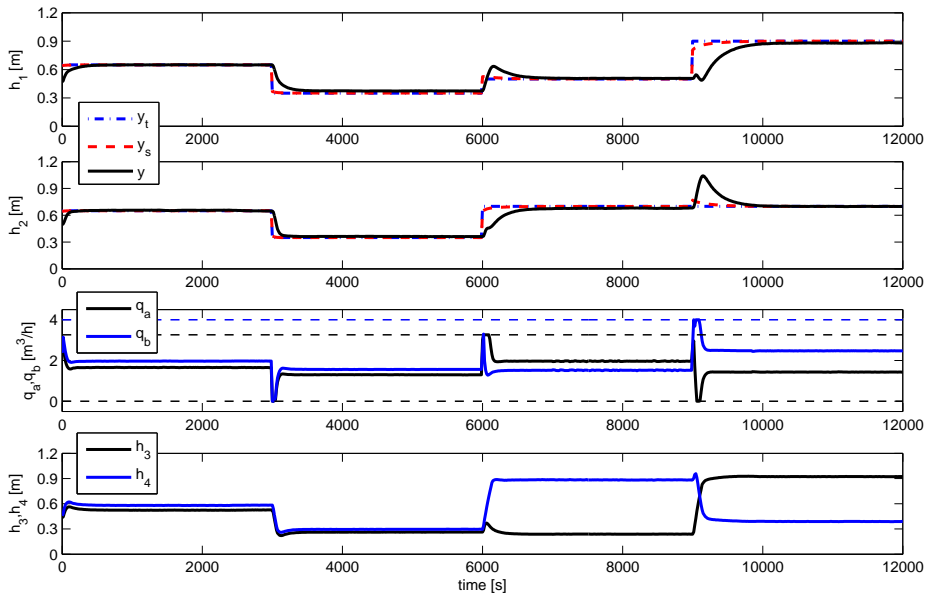
- ▶ Initial condition: $x_0 = (0.47, 0.49, 0.44, 0.46)$.
- ▶ 4 changes of reference: $y_{t,1} = (0.65, 0.65)$, $y_{t,2} = (0.35, 0.35)$, $y_{t,3} = (0.50, 0.70)$ and $y_{t,4} = (0.90, 0.70)$.
- ▶ MPC setup: $N=5$, $Q = I_4$, $R = 0.01I_2$, $w_{1,2} = 0.5$.
- ▶ $K = K_{LQR}$. P : solution of the Riccati equation.
- ▶ $V_O(y_s, y_t) = \|y_s - y_t\|_T^2$ where $T = 100I_2$.
- ▶ $\bar{p} = 1$.
- ▶ Constraints:

	Value	Unit	Description
H_{1max}	1.36	m	Maximum level of the tank 1
H_{2max}	1.36	m	Maximum level of the tank 2
H_{3max}	1.30	m	Maximum level of the tank 3
H_{4max}	1.30	m	Maximum level of the tank 4
H_{min}	0.2	m	Minimum level in all cases
V_{max}	0.2226	m^3	Maximum water volume
Q_{amax}	3.26	m^3/h	Maximum flow of pump A
Q_{bmax}	4	m^3/h	Maximum flow of pump B
Q_{min}	0	m^3/h	Minimal flow

Experiment: results



Experiment: results (2)



Summary

Cooperative distributed MPC for tracking.

- ▶ Players share a common objective.
- ▶ Centralized offset cost function and terminal constraint.
- ▶ Feasibility ensured for any changing setpoint.
- ▶ Convergence to the centralized optimum ensured for any $\bar{\rho} \geq 1$.
- ▶ Domain of attraction larger than standard MPC.

Future works:

- ▶ Economic offset cost function: DMPC+RTO, incremental model.
- ▶ Distributed terminal constraint (Conte et al., 2012; Rakovic et al., 2010).
- ▶ Nonlinear cooperative MPC for tracking.
- ▶ Offset free.

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Thanks for your attention!